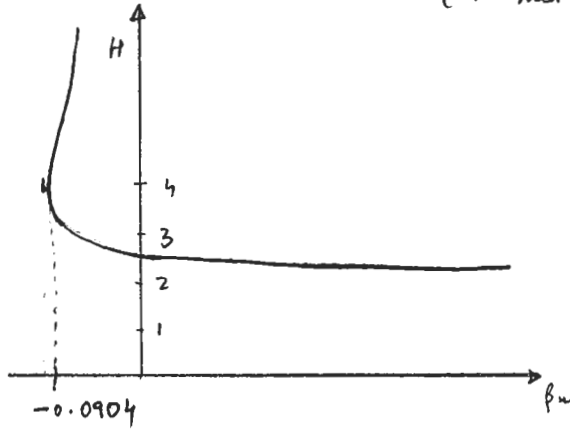


1,2 > β_w is minimum when $H=4$ ($\beta_{w, \min} = -0.0904$)



No solution exists for $\beta_{w, \text{spec}} < \beta_{w, \min}$, so Newton method oscillates back and forth without converging

$$3 > U_w = - \frac{\partial \Psi}{\partial x} \Big|_{y=0} = - \frac{\partial}{\partial \xi} (MF) + \frac{\eta}{\Delta} \cdot \frac{dA}{d\xi} \frac{\partial}{\partial \eta} (MF) = -M \frac{\partial F}{\partial \xi} - F \frac{dM}{d\xi} = - \frac{M}{2} \beta_w F$$

$$\frac{\partial F}{\partial \xi} = 0 \rightarrow \text{similar flow}$$

$$V_w \equiv \sum \frac{v_{wall}}{m} = \sum \frac{v_{wall}}{A u_e} = -\beta_w F(0) = - \left(\frac{\beta_w + 1}{2} \right) F(0)$$

Modified b.c.s :

$$a > U_w = U_{w, \text{spec}} \Rightarrow R_{BC2} \equiv U_1 - U_{w, \text{spec}} = 0$$

$$b > V_w = V_{w, \text{spec}} \Rightarrow R_{BC1} \equiv \frac{\beta_w + 1}{2} F(0) - V_{w, \text{spec}} = 0$$

3a > Solving for $H(\beta_w)$ for a range of U_w produces $U_w = 0.415$ when $\beta_w = -0.18$

3b > Solving for $H(\beta_w)$ for a range of V_w produces $V_w = -0.345$ when $\beta_w = -0.18$.

A direct approach would be to make U_w and V_w global variables. Augment the right hand side with another column vector $\{\partial \vec{R} / \partial U_w\}$

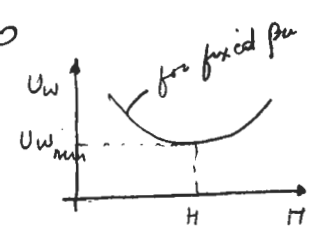
$$\Rightarrow \begin{bmatrix} \frac{\partial \vec{R}}{\partial (F, U, S)} \end{bmatrix} \begin{Bmatrix} \delta F \\ \delta U \\ \delta S \end{Bmatrix} = -\{\vec{R}\} - \delta U_w \begin{Bmatrix} \partial \vec{R} \\ \partial U_w \end{Bmatrix}, \quad \begin{Bmatrix} \partial \vec{R} \\ \partial U_w \end{Bmatrix} = \begin{Bmatrix} -1 \\ 0 \\ \vdots \end{Bmatrix} \leftarrow \text{RHS}$$

$$\begin{bmatrix} \partial R_p / \partial (F, U, S) \end{bmatrix} \begin{Bmatrix} \delta U_w \end{Bmatrix} = \begin{Bmatrix} -R_p \end{Bmatrix} - \delta U_w \begin{Bmatrix} \partial R_p / \partial U_w \end{Bmatrix}, \quad \begin{Bmatrix} \partial R_p / \partial U_w \end{Bmatrix} = \begin{Bmatrix} 0 \end{Bmatrix}$$

new variable

Solve for $\delta F_i, \delta U_i, \delta S_i, \delta U_w$ and update

Since $\rho u = f(U_w, H) = -0.18$, $\delta \rho u = \frac{\partial \rho u}{\partial H} dH + \frac{\partial \rho u}{\partial U_w} dU_w = 0$

$$\Rightarrow \frac{dU_w}{dH} = - \frac{\partial \rho u / \partial H}{\partial \rho u / \partial U_w}$$


which is 0 when U_w is a minimum, since $\partial \rho u / \partial H = 0$.
Same approach can be applied to calculate V_w as a global variable

3c) $Re = 10^6 = \frac{U_{\infty} c}{\nu}$, $U_{wall} = V_{wall} \cdot V_c \approx U_{wall} \cdot U_{\infty} = 0.415 U_{\infty}$ (large, 40% of U_{∞})

$$V_{wall} = V_{U_c} \frac{\Delta}{c} \approx -0.345 U_{\infty} \sqrt{\frac{\nu}{U_{\infty} c}} = -0.000345 U_{\infty}$$

$\therefore V_w$ is more reasonable
 \Rightarrow suction is more feasible/practical

4) Boundary layer suction ($U_w \neq 0, \nu_w = 0$) is applied on the upper surface of an airfoil to suppress separation

$$u_e(x) \approx U_{\infty} (x/c)^{-0.09}$$

a, for similarity, $V_w = \text{constant}$

$$= \frac{V_w \frac{x}{c}}{m} \quad \text{or} \quad V_w = V_w \cdot \frac{m}{\frac{x}{c}} = \text{const.} \cdot \left(\frac{x}{c}\right)^{-(\beta m - 1)/2}$$

On the airfoil $V_w(x) = \text{const.} \cdot \left(\frac{x}{c}\right)^{(\beta m - 1)/2} = \text{const.} \cdot \left(\frac{x}{c}\right)^{-0.545}$

467 $\beta u = -0.09$, $Re_c = 10^6$

$$\frac{\theta}{c} \Big|_{t.o} = \theta_1 / \sqrt{Re_c}, \quad C_{D,prof} = 2 \left[\left(\frac{\theta}{c} \right)_u + \left(\frac{\theta}{c} \right)_L \right]_{t.e}$$

$$= \frac{2}{\sqrt{Re_c}} \left[\theta_{1,u} (V_w) + \theta_{1,L} \right], \quad \theta_{1,L} = 0.567$$

($\alpha = \beta u = -0.09$)

On the upper surface

$$\frac{V_w(x)}{U_\infty} = \frac{V_w}{\sqrt{Re_c}} \cdot (x/c)^{-1/2} \cdot \left(\frac{Uc}{U_\infty} \right)^{1/2}$$

$$= \frac{V_w}{\sqrt{Re_c}} (x/c)^{-1/2} (x/c)^{\beta u/2} = \frac{V_w}{\sqrt{Re_c}} (x/c)^{-\frac{1}{2}(\beta u - 1)}$$

Define suction coefficient

$$C_s = \int_0^c \frac{\rho V_w dx}{\rho U_\infty c} = \int_0^1 \left(\frac{V_w}{U_\infty} \right) d(x/c) = \frac{V_w}{\sqrt{Re_c}} \left(\frac{\beta u + 1}{2} \right)$$

The power required to pump the suctioned boundary layer fluid back to free stream stagnation pressure

$$P_{suction} = \int_0^c \frac{\Delta P_e}{\rho} \cdot dm_{suction} = \int_0^c \frac{(P_{t_\infty} - P_e)}{\rho} dm_{suction}$$

$$P_{t_\infty} - P_{t_c} = \frac{1}{2} \rho U_\infty^2$$

$$\therefore P_{suction} = \int_0^c \frac{1}{2} \rho U_\infty^2 dm_{suction} \quad (> 0)$$

$$C_{P,suction} = \frac{P_{suction}}{\frac{1}{2} \rho U_\infty^3 \cdot c} = \int_0^1 \left(\frac{Uc}{U_\infty} \right)^2 \left(\frac{|V_w|}{U_\infty} \right) d(x/c) \quad (> 0)$$

$$= \int_0^1 (x/c)^{2\beta u} \cdot \frac{|V_w|}{\sqrt{Re_c}} \cdot (x/c)^{-\frac{1}{2}(\beta u - 1)} d(x/c)$$

$$= \frac{|V_w|}{\sqrt{Re_c}} \int_0^1 (x/c)^{\frac{5\beta u - 1}{2}} d(x/c) = \frac{|V_w|}{\sqrt{Re_c}} \cdot \left(\frac{5\beta u + 1}{2} \right)$$

$$\therefore C_{p \text{ suction}} = |C_a| \left(\frac{5\beta u + 1}{\beta u + 1} \right)$$

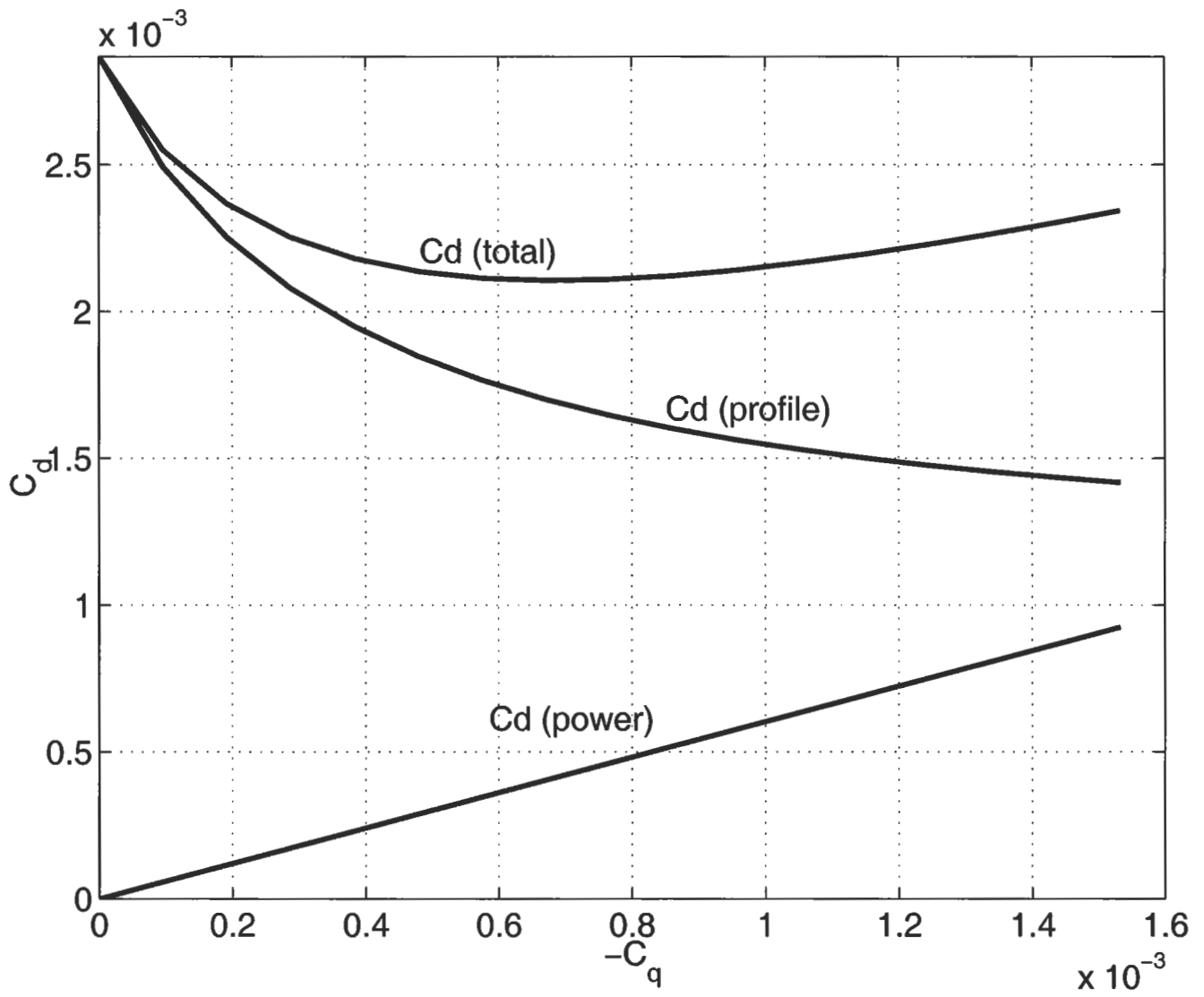
$$\beta u = -0.09 \Rightarrow C_{p \text{ suction}} = |C_a| 0.604.$$

The total drag is then

$$D = D_{\text{prof}} + \frac{P_{\text{suction}}}{U_{\infty}}$$

$$C_D = C_{D \text{ prof}} + C_{p \text{ suction}} //$$

Min. C_D occurs at $C_D \approx 0.9 \times 10^{-3}$ (see attached plot)



```

C
C
C
C
C---- wall BC equation matrix entries, put into 1,2 equations of i=1 block row
I = 1
R(1,1,I) = F(I) + VWALL*2.0/(1.0 + BU)
A(1,1,I) = 1.0
R(1,2,I) = - VWALL*2.0/(1.0 + BU)**2
C
R(2,1,I) = U(I) - UWALL
A(2,2,I) = 1.0
C
C---- set up equations for each i..i+1 interval
DO 12 I = 1, N-1
  BCON = 0.5*(1.0 + BU)
  DETA = ETA(I+1) - ETA(I)
C
C----- set S-equation matrix entries, put into 3rd equation of I block row
R(3,1,I) = S(I+1) - S(I) ! Residual
& + BCON*0.5*DETA*(F(I+1)*S(I+1) + F(I)*S(I))
& + BU*DETA*(1.0 - 0.5*(U(I+1)**2 + U(I)**2))
C
C(3,1,I) = BCON*0.5*DETA* S(I+1) ! dR/dF(i+1)
A(3,1,I) = BCON*0.5*DETA* S(I) ! dR/dF(i)
C
C(3,2,I) = BU*DETA*( - U(I+1) ) ! dR/dU(i+1)
A(3,2,I) = BU*DETA*( - U(I) ) ! dR/dU(i)
C
C(3,3,I) = 1.0 ! dR/dS(i+1)
& + BCON*0.5*DETA* F(I+1)
A(3,3,I) = - 1.0 ! dR/dS(i)
& + BCON*0.5*DETA* F(I)
C
R(3,2,I) = 0.25*DETA*(F(I+1)*S(I+1) + F(I)*S(I)) ! dR/dBetau
& + DETA*(1.0 - 0.5*(U(I+1)**2 + U(I)**2))
C
C----- set F equation matrix entries, put into 1st equation of I+1 block row
R(1,1,I+1) = F(I+1) - F(I) - 0.5*DETA*(U(I+1) + U(I)) ! Residual
A(1,1,I+1) = 1.0 ! dR/dF(i+1)
B(1,1,I+1) = - 1.0 ! dR/dF(i)
A(1,2,I+1) = - 0.5*DETA ! dR/dU(i+1)
B(1,2,I+1) = - 0.5*DETA ! dR/dU(i)
C
C----- set U equation matrix entries, put into 2nd equation of I+1 block row
R(2,1,I+1) = U(I+1) - U(I) - 0.5*DETA*(S(I+1) + S(I)) ! Residual
A(2,2,I+1) = 1.0 ! dR/dU(i+1)
B(2,2,I+1) = - 1.0 ! dR/dU(i)
A(2,3,I+1) = - 0.5*DETA ! dR/dS(i+1)
B(2,3,I+1) = - 0.5*DETA ! dR/dS(i)
C
12 CONTINUE
C
C---- edge BC equation matrix entries, put into 3rd equation of i=N block row
I = N
R(3,1,I) = U(I) - 1.0
A(3,2,I) = 1.0
C
C
C
C
C
C
C

```

```

C
C
RBETA = 0.
RB_R1 = 0.
RB_R2 = 0.
C
---- accumulate Rbeta, dR/dU(i).r(i), dR/dU(i).s(i) from each interval
DO 16 I = 1, N-1
  DETA = ETA(I+1) - ETA(I)
  UAV = 0.5*(U(I) + U(I+1))
C
C----- set RBETA increment, and its derivative with respect to UAV
DRB      = (1.0-UAV)*DETA - HSPEC*(UAV - UAV**2)*DETA
DRB_UAV =      -      DETA - HSPEC*(1.0 - UAV*2.0)*DETA
C
C----- derivatives of RBETA with respect to U(i), U(i+1)
DRB_UO = DRB_UAV*0.5
DRB_UP = DRB_UAV*0.5
C
C----- accumulate RBETA, and RBETA changes resulting from R(.1.) and R(.2.)
RBETA = RBETA + DRB
RB_R1 = RB_R1 + DRB_UO*R(2,1,I) + DRB_UP*R(2,1,I+1)
RB_R2 = RB_R2 + DRB_UO*R(2,2,I) + DRB_UP*R(2,2,I+1)
16 CONTINUE
C
C---- require RBETA + d(RBETA) = 0
C-      or RBETA - RB_R1 - RB_R2*DBU = 0
C
DBU = (RBETA - RB_R1) / RB_R2

```