

Gibbs method - takes advantage of constraints ①
 from thermo. equilib. & mass balance.

equilib. constraints

$$\sum_{j=1}^m \nu_j \mu_j = 0$$

$$\Delta G_{\text{rxn}} = 0$$

one for every stoichiometric equation
 written among the phase components
 of an equilibrium assemblage.

only necessary to write a linearly independent
 subset of all the possible reactions.

$$\# \text{ of linearly indep. reactions} = \begin{matrix} \text{Total} \\ \# \text{ of phase} \\ \text{components} \\ \text{in all phases in} \\ \text{an assembl.} \end{matrix} - \# \text{ of system components}$$

- stoichiometric constraints

$$\sum_{j=1}^{n_{pc}^k} X_j^k = 1 \leftarrow X_j^k \text{ is the mole frac. of component } j \text{ in phase } k$$

- mass balance constraint

one for each independent system component
 specifies the bulk comp. of the rock by describing
 the amt. of each component present

$$m_i = \sum_{k=1}^{n_{ph}} n_i^k M^k \leftarrow \begin{matrix} \text{one for} \\ \text{each} \\ \text{component} \end{matrix} \quad \begin{matrix} n_i^k = \# \text{ of moles of} \\ \text{sys comp. } i \text{ in} \\ \text{phase } k. \\ M^k = \# \text{ of moles of } k \\ \text{in the rock} \end{matrix}$$

m_i - the number of moles of system component i is generally known, because it defines the bulk composition

the variable n_i^k can be expressed in terms of

X_j^k - it is the sum of the # of moles of system component i in one mole of each phase component j - $(n_{i,j}^k) \times$ the mole fraction of phase component j in the mineral or melt... X_j^k

or

$$n_i^k = \sum_{j=1}^{n_{pck}} n_{i,j}^k X_j^k$$

and the full mass balance becomes

$$m_i = \sum_{k=1}^{n_{ph}} M^k \sum_{j=1}^{n_{pck}} n_{i,j}^k X_j^k$$

intensive variables in the Gibbs minimization of free energy are T, P and μ

the number of independent variables is given by the Gibbs phase rule

$$F = n_{sc} + 2 - n_{ph}$$

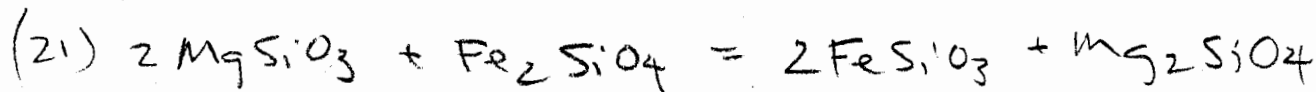
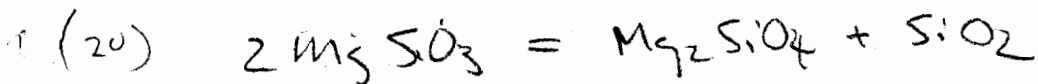
for system $MgO - FeO - SiO_2$

(4)

phase components

Qtz
OPX
Oliv

2 linearly independent reactions



conditions of equilib.

$$(20) \quad -RT \ln K_{20} = \Delta H_{298} + \int_{298}^T \Delta C_p dT + \int_P^2 \Delta V dP - T \left(\Delta S_{298} + \int_{298}^T \frac{\Delta C_p}{T} dT \right)$$

$$(21) \quad -RT \ln K_{21} = \dots$$

Stoichiometric constraints

$$X_{SiO_2}^{Qtz} = 1$$

$$X_{Fa}^{ol} + X_{Fo}^{ol} = 1$$

$$X_{En}^{opx} + X_{Fs}^{opx} = 1$$

of intensive variables = ?

$$T, P, X_{Fo}, X_{Fa}, X_{En}, X_{Fs}, X_{SiO_2}$$

of constraints = 5

\therefore 2 degrees of freedom

also mass balance constraints

$$M_{SiO_2} = m_{Qtz} + M^{ol} (X_{Fo}^{ol} + X_{Fa}^{ol}) + M^{opx} (X_{En}^{opx} + X_{Fs}^{opx})$$

$$M_{FeO} = 0 + M^{ol} (2X_{Fa}) + M^{opx} (X_{Fs})$$

so the total # of constraints (5)
 thermodynamic (2)
 stoichiometric (3)
 mass balance (3)

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Total # of variables
 T, P
 X_{qtz}
 X_{px}
 E_i
 X_{fs}
 X_{fo}
 X_{fo}
 M_{FeO}
 M_{MgO}
 M_{SiO₂}

(10)

for a variance of 2 - so - any
 2 variables can be taken as independent

$$F = C + 2 - \phi = 5 - 3 = 2$$

now - what to do with all of this information

- 1) choose variables as independent = to the variance
- 2) specify values for each independent variable
- 3) solve for dependent variables

we have been doing this graphically throughout the semester

showing a T-X diagram and fixing P [⊙]

choosing T and X as independent variables

solving series of non-linear equations

to use Newton-Raphson - need to take total derivative of each equation with respect to the independent variables, e.g. T, P, X_j

so for each μ_i in our stoichiometric constraints

$$\sum_{j=1}^m \nu_j \mu_j, \quad \left. \frac{\partial \mu_j}{\partial T} \right|_{P, X} = -\bar{S}_j$$

$$\left. \frac{\partial \mu_j}{\partial P} \right|_{T, X} = \bar{V}_j$$

$$\left. \frac{\partial \mu_j}{\partial X_i} \right|_{T, P, X_i \neq X_j} = \frac{RT \alpha_j}{X_j} + \frac{RT \alpha_j}{\gamma_j} \left(\frac{\partial \gamma_j}{\partial X_i} \right)_{T, P, X_i \neq X_j}$$

since the non-ideal

term $RT \ln \gamma_j$ is a function of the composition of the phase - all the other X_j's

change its value

$$\left. \frac{\partial \mu_j}{\partial X_i} \right|_{T, P, X_i \neq X_j} = \frac{RT \alpha_j}{\gamma_j} \left. \frac{\partial \mu_j}{\partial X_i} \right|_{T, P, X_i \neq X_j}$$

②

plug these constraints into the original
2 stoic. coefficients

$$-AS dT + \Delta V dP + \sum_{j=1}^m V_j \frac{RT\alpha_j^0}{x_j} dx_j$$

$$+ \sum_{j=1}^m V_j \left[\sum_{i=1}^{npct} \frac{RT\alpha_j}{V_j} \frac{\partial x_j}{\partial x_i} \Big|_{T,P, x_j \neq x_j} \right] dx_i$$

stoic constraints

$$\sum_{j=1}^{npck} dx_j^k = 0$$

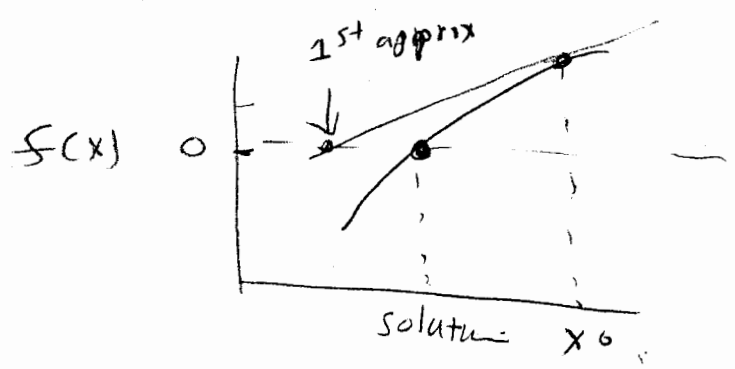
mass balance constraints for a closed system

$$\sum_{k=1}^{nph} M^k \sum_{j=1}^{npck} n_{ij}^k dx_j^k + \sum_{k=1}^{nph} dM_k \sum_{j=1}^{npck} n_{ij}^k x_j^k$$

solve using Newton-Raphson

find $f(x) = 0$

where $f(x) = f(x^0) + \frac{\partial f(x^0)}{\partial x} \Delta x$



p. 562 - shows it for
our system

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two variables must be specified

after $T \hat{=} P$, but not necessary

might be better to specify $P \hat{=} \text{bulk comp.}$

for the ex. in Spear -

he chooses T and X_{Fs}^{Px} and solves

for pressure and comp. of olivine and

mols of qtz, Px and oliv - assembl.

substitute in for $\Delta T = \Delta X_{Fs} = 0$

16-2 shows resulting equations

Jacobian soln method useful if

you don't have complete thermob.

Table 16-5 shows problem where
the trivial constraint for qtz has
been relaxed.

Spec construction

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T-X, P-X and P-T diagrams

rearrange eqns in 16-6 to show selected dependent variable

need to fix x_{Fs} and the start at a reference condition

16-2 shows P-X, T-X and T-P

diagrams

18.571

when you add mass balance constraints always have 2 degrees of freedom

— can track reactions completely

16-4 - shows molar properties

for fixed molar properties

p_x used up first on decompression

dlu used up first on cooling