3.091 OCW Scholar

Self-Asessment

Reactions and Kinetics

Supplemental Exam Problems for Study

Solutions Key

Acetaldehyde, CH₃CHO, will decompose into methane and carbon monoxide according to

$$CH_3CHO(g) \Rightarrow CH_4(g) + CO(g)$$

At 450°C the rate of consumption of CH₃CHO is measured to vary with the concentration of CH₃CHO raised to the power 1.5.

(a) With a CH₃CHO concentration of 0.222 M, the rate of consumption of CH₃CHO at 450°C is measured to be 3.33×10^{-3} Ms⁻¹. Calculate the rate of production of carbon monoxide when the concentration of CH₃CHO has fallen to 0.111 M.

=)CHCHC Ø nt of prodof CH2CHO $= \frac{-3}{(0.111)} = 1.18 \times 10$

(b) On the graph below, show how the specific chemical rate constant, k, varies with temperature when the above reaction is conducted **1** in the absence of a catalyst; and **2** in the presence of a catalyst. Label both lines so as to associate each with either **1** or **2**. The diagram is not to be drawn to scale; however, you must pay attention to relative magnitudes.



3.091 Fall Term 2007 Test #3

Problem #6

- (a) A specimen of LaNi₅ containing hydrogen is placed in a vacuum furnace. After 1 hour, at what depth from the surface of the specimen has the concentration of hydrogen reached $\frac{1}{3}$ the initial concentration? The diffusion coefficient of hydrogen in the alloy has a value of 3.091×10^{-6} cm² s⁻¹. Assume that the initial concentration of hydrogen is uniform throughout the specimen and that the concentration of hydrogen is maintained at zero in the vacuum furnace.
 - DATA: Error Function Values (given without regard as to whether you need these data to solve the problem)
 - for values of $\xi < 0.6$, use the approximation $erf(\xi) = \xi$; erf(1.0) = 0.843; erf(2.0) = 0.998



(b) On the same graph below, sketch the profiles of $\mathbf{0}$ the concentration of hydrogen, $c_{\rm H}$, and $\mathbf{2}$ the absolute magnitude of the flux of hydrogen, $|J_{\rm H}|$, in the near-surface region of the specimen of part (a) at time, t_1 , where $0 < t_1 < 1$ h.



Azomethane, $CH_3N_2CH_3$, decomposes at 600 K to ethane, C_2H_6 , and nitrogen, N_2 . The reaction has been measured to be first order in azomethane.

(a) Write the rate law expression for the decomposition of azomethane.

t=kc where c=2CH3 N2 CH3

(b) The value of the half-life, t_{λ_2} , for this reaction has been measured to be 1920 s. How much of the initial amount of azomethane remains after 3.091 h? Express your answer as a *fraction* of the initial concentration, c_0 , of azomethane.

lu c/c, = - let for 1st order rxns & = 0.693/tiz $c_{c} = exp - \frac{0.693}{t_{1/2}} t = exp - \frac{0.693 \times 3.091 \times 3600}{1920} = 1.60 \times 10^{-10}$ 3.091 h = (3.091×3600)/1920 = 5.8 Malf lives $C_{0} = (-1)^{S, o}$

(c) On the plot below, sketch the variation in energy (\approx chemical potential) with extent of reaction for the decomposition of azomethane. Assume that the ratio of $E_a/\Delta E_{\text{reaction}} = -3$, where E_a represents the activation energy and $\Delta E_{\text{reaction}}$ the energy change of the reaction. Label E_a and $\Delta E_{\text{reaction}}$. Label the energy states of CH₃N₂CH₃, C₂H₆, and N₂.



extent of reaction

(d) How does a catalyst change the ratio of the absolute value of $E_a/\Delta E_{\text{reaction}}$? Increase? Decrease? No change? Justify your answer by explaining what happens at the atomic level in the catalysis of a reaction in which all the reactants and products are gases.

decrease catalyst reduces The activation barrier at The atomistic level The actulyst adsorbs CH_W_CH_ and facilitates breaking the N=N double tind

There is a differential nitrogen pressure across a furnace wall made of steel measuring 2.22 mm in thickness. The concentration of nitrogen at the inner surface of the wall is held constant at 9.99 kg m⁻³, while the concentration at the outer surface of the wall is held constant at 1.11 kg m⁻³. The area of the wall is 3.33 m², and the diffusivity of nitrogen in steel at the furnace operating temperature is $D_{\rm N} = 3.091 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$.

(a) What is the total rate loss of nitrogen from the furnace at steady state? Express your answer in units of kg s⁻¹.

 $\frac{dm}{dt} = \sqrt{A} = \left(-\frac{D}{dx}\right)A = -\frac{D}{\Delta A} = -\frac{D}{\Delta X} \qquad \begin{array}{l} now \ neglect \\ minus \ sign \\ = 3.091 \times 10^{-10} \times 3.33 \times \frac{(9.99 - 1.11)}{2.22 \times 10^{-3}} = 4.12 \times 10^{-6} \ kg/s \end{array}$

(b) If the steel of the wall were replaced with another steel of the identical composition but with a grain size 10× larger than that of the steel in part (a), how would the loss of nitrogen from the furnace change? Explain.

as grain size increases, The ratio of grain bodry to bulk SECREASES. Since Dulk < Dgb, to decrease

(a) The energy of vacancy formation, ΔH_v , in palladium (Pd) is 1.5 eV. At 888°C there is one vacancy for every million (10⁶) atom sites. Is it possible, by simply raising the temperature and *not exceeding the melting point of the metal*, to achieve a vacancy fraction of one vacancy for every thousand (10³)

atom sites? + which Conve 10 16 Conve Pd = 1882°C > m.p. using data get value of A Answer: NO! at EBOC 1161

(b) You are given two specimens of Pd, each of identical purity. Specimen **①** has a grain size of 3.091 μm; specimen **②** has a grain size of 444 μm. Which specimen will exhibit a higher rate of diffusion of hydrogen through it? Explain the reason for your choice.

The diffusivity of hydrogen will be orders of magnitude higher along the grain boundaries of Pd than through the bulk of the crystal. Hence, the specimen with more grain boundary per unit volum will exhibit a higher rate of hydrogen permeation. Assuming that the width of the grain boundary is invariant with grain size, specimen **1** will have more grain boundary per unit volume and therefore a higher rate of hydrogen permeation.

Problem #10 (7 points)

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Sulfuryl chloride, SO₂Cl₂, decomposes to SO₂ and Cl₂ according to

 $SO_2Cl_2(g) \rightarrow SO_2(g) + Cl_2(g).$

The reaction is first order in SO₂Cl₂, and the value of the rate constant, *k*, is 2.2×10^{-5} s⁻¹.

(a) Calculate the initial rate of reaction when a reactor is charged with SO_2Cl_2 at a concentration of 0.11 mol L⁻¹. Express your answer in units of mol L⁻¹ s⁻¹.

$\frac{dc}{dt} = -kc = 2.2 \times 10 \times 0.11 = 2.42 \times 10^{-10}$

(b) Calculate how long it will take for the concentration of SO_2Cl_2 in the reactor in part (a) to fall to ¹/₄ of its initial value. Express your answer in units of s.

 $\frac{1}{2} = \frac{1}{12} \neq u \neq u \neq u \neq u \neq u \neq u \neq 2$ $\frac{1}{2} ha + 1 + 1 + v \neq S = 6.30 \times 10^{7} \text{ s}$ $\frac{1}{2} ha + 1 + 1 + v \neq S = 6.30 \times 10^{7} \text{ s}$ $\frac{1}{2} ha + 1 + 1 + v \neq S = 6.30 \times 10^{7} \text{ s}$ méthod (; Calculate 4 6.30×1045

(a) The diffusion coefficient of oxygen in silicon, D_0 , has been measured to have the following values:

$D_{\rm O}~({\rm cm}^2~{\rm s}^{-1})$	T (°C)
9.2×10^{-11}	1100
1.4×10^{-9}	1300

Show that in order to increase the value of D_0 by a factor of 10× greater than it is at 1300°C would require raising the temperature above the melting point of silicon.

$$\begin{split} D &= \int_{0}^{\infty} e^{\chi} p - \frac{Q}{RT} \implies find T \text{ of which } D &= 10 \times \int_{1300}^{1300} \frac{Q}{RT} = 10 \times \int_{1300}^{1300} \frac{Q}{RT} = 10 \times \int_{1300}^{1300} \frac{Q}{RT} = 10 \times \int_{1300}^{14} \frac{Q}{RT} = 10 \times \int_{140}^{14} \frac{Q}{RT}$$

(b) Make a crude estimate showing that it is feasible to remove oxygen from a silicon ribbon of thickness $0.1 \,\mu\text{m}$ by exposing the ribbon to vacuum for 10 minutes at a temperature of 1100°C.

 $\chi^2 \approx \mathcal{J} = 9.2 \times 10^{-11} \times 10 \times 60 = 5.5 \times 10^{-8} \text{ cm}^2$: $\chi = 2.35 \times 10^{-0} \text{ cm} = 2.35 \text{ µm} > 0.1 \text{ µm}$

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