# **Brayton Cycle Summary**

define some units

$$kJ := 10^3 \cdot J$$



Gas Turbine represented by air standard Brayton cycle

Brayton cycle consists of:

1-2 adiabatic compression

2-3 heat addition ~ constant pressure

3-4 adiabatic expansion in turbine

4-1 heat rejection ~ constant pressure

p-v and T - s plots for Brayton cycle shown below for reversible cycle. in irreversible cycle,  $p_2 > p_3$  and  $p_4 > p_1$ ,  $s_2 > s_1$ ,  $s_4 > s_3$ 

starting conditions	$p_{1_plot} := 1$	$T_{1_plot} := 25 + 273.15$	$s_{1_plot} := 1$
after compression	panaloti = 10		
max temperature after heat addition	$T_{3_{plot}} := 1000 + 27$	73.15	

**D** calculations







# Ideal (reversible) basic Brayton cycle

$$\begin{array}{ll} \mbox{compressor work} & w_c = -(h_2 - h_1) & \mbox{heat addition} & q_H = h_3 - h_2 \\ \mbox{turbine work} & w_t = h_3 - h_4 & \mbox{heat rejection} & q_L = -(h_4 - h_1) \\ & \eta_{th} = \frac{q_H + q_L}{q_H} = 1 + \frac{q_L}{q_H} = \frac{w_t + w_c}{q_H} \\ & h_{4s} := C_p \left(T_{4s} - T_1\right) + h_1 & \mbox{assuming perfect gas, constant specific heat.} \\ & h_{3s} := C_p \left(T_3 - T_{2s}\right) + h_{2s} & \mbox{assuming perfect gas, constant specific heat.} \\ & h_{3s} := C_p \left(T_3 - T_{2s}\right) + h_{2s} & \mbox{assuming perfect gas, constant specific heat.} \\ & (1) & \eta_{th} := 1 - \frac{h_{4s} - h_1}{h_3 - h_{2s}} & \eta_{th} \rightarrow 1 - \frac{T_{4s} - T_1}{T_3 - T_{2s}} & \eta_{th} := 1 - \frac{T_1}{T_{2s}} - \frac{T_4}{T_{2s}} - \frac{T_4}{T_{2s}} \\ & \mbox{is is reversible adiabatic process with ideal gas and constant specific heat} \\ & \mbox{since} & \frac{P_{2s}}{P_1} = \frac{P_3}{P_{4s}} & \frac{T_{2s}}{T_1} = \left(\frac{p_{2s}}{P_1}\right)^{\frac{\gamma}{\gamma}} = \left(\frac{p_{2s}}{P_{4s}}\right)^{\frac{\gamma-1}{\gamma}} \\ & \mbox{is is reversible adiabatic process with ideal gas and constant specific heat} \\ & \mbox{n}_{th} = 1 - \frac{T_1}{T_{2s}} = 1 - \left(\frac{p_1}{P_{2s}}\right)^{\frac{\gamma-1}{\gamma}} \\ & \mbox{is is reversible adiabatic process with ideal gas and constant specific heat} \\ & \mbox{n}_{th} = 1 - \frac{T_1}{T_{2s}} = 1 - \left(\frac{p_1}{P_{2s}}\right)^{\frac{\gamma-1}{\gamma}} \\ & \mbox{is is reversible adiabatic process with ideal gas and constant specific heat} \\ & \mbox{n}_{th} = 1 - \frac{T_1}{T_{2s}} = 1 - \left(\frac{p_{2s}}{P_{2s}}\right)^{\frac{\gamma-1}{\gamma}} \\ & \mbox{is is reversible adiabatic process with ideal gas and constant specific heat} \\ & \mbox{n}_{th} = 1 - \frac{T_1}{T_{2s}} = 1 - \left(\frac{p_{2s}}{P_{2s}}\right)^{\frac{\gamma-1}{\gamma}} \\ & \mbox{is is reversible adiabatic process with ideal gas and constant specific heat} \\ & \mbox{n}_{th} = 1 - \frac{T_1}{T_{2s}} = 1 - \frac{q_{1s}}{T_{1}} = \frac{T_{2s}}{T_{2s}} \\ & \mbox{is is reversible adiabatic process with ideal gas and constant specific heat} \\ & \mbox{is is reversible adiabatic process with ideal gas and constant specific heat} \\ & \mbox{n}_{th} = 1 - \frac{T_1}{T_{2s}} = 1 - \frac{T_1}{T_{2s}} = 1 - \frac{T_1}{T_{2s}} + \frac{T_1}{T_{2s}} = 1 - \eta_{1s}$$

monotonic gasses, He, Ar, Ne, He

$$\eta_{\text{th}} \coloneqq 0.5$$
  $i \coloneqq 0..2$   
 $r_i \coloneqq (1 - \eta_{\text{th}})^{\frac{-\gamma_i}{\gamma_i - 1}}$   $r = \begin{pmatrix} 21.83 \\ 11.31 \\ 5.63 \end{pmatrix}$ 

so for air as the working fluid, a pressure ratio of 11.3 will provide 0.5 isentropic efficiency

 $\frac{-\gamma}{\gamma-1}$ 

effect of pressure ratio on isentropic efficiency

$$\mathfrak{m}_{\mathsf{the}}(\mathbf{r},\gamma) := 1 - \frac{1}{\frac{\gamma - 1}{r}} \qquad \mathfrak{m} := 0 \dots 25 \qquad \qquad \gamma = \begin{pmatrix} 1.29 \\ 1.4 \\ 1.67 \end{pmatrix}$$



pressure ratio



$$\eta_{\text{th}} = 1 + \frac{w_{\text{c}}}{w_{\text{t}}} = 1 - \frac{c_{\text{p}} \cdot (T_2 - T_1)}{c_{\text{p}} \cdot (T_3 - T_4)} = 1 - \frac{T_1 \cdot \left(\frac{T_2}{T_1} - 1\right)}{T_3 \cdot \left(1 - \frac{T_4}{T_3}\right)} = \frac{T_1 \cdot \left[\left(\frac{p_2}{p_1}\right)^{\gamma} - 1\right]}{T_3 \cdot \left[1 - \left(\frac{p_1}{p_2}\right)^{\gamma}\right]} \quad \text{as ... p1/p2 = p4/p3}$$

form is ... 
$$\frac{\frac{a^{b}-1}{1-\frac{1}{a^{b}}} = \frac{a^{b}-1}{\frac{a^{b}-1}{a^{b}}} = a^{b}}{\eta_{th}} = 1 - \frac{T_{1}}{T_{3}} \cdot \left(\frac{p_{2}}{p_{1}}\right)^{\gamma} \quad Q.E.D.$$

for example, plot  $\eta_{th}$  vs pr for  $\gamma$  = 1.4 (air) with regeneration and T1/T3 = 0.25  $\,$  figure 9.27  $\,$ 

$$\gamma := 1.4$$
  $r := 1..14$   $T1_over_T3 := 0.25$   $\eta_{th_reg}(r, \gamma, T1_over_T3) := 1 - T1_over_T3 \cdot r^{\gamma}$ 

11/14/2005



----- air - gamma = 1.4 with regen. T3/T1=4

 $\dot{w} = 2$  solve for pressure ratio at intersection

Given

$$\eta_{\text{th}_{reg}}(r,\gamma,T1_{over}_{T3}) = \eta_{\text{th}}(r,\gamma)$$

 $\begin{array}{ll} r\_intersect \coloneqq Find(r) & r\_intersect = 11.314\\ \text{say} \ldots & T_1 \coloneqq 300 & T_3 \coloneqq 1200\\ \text{at this pressure ratio} \end{array}$ 

$$T_2 \text{ intersect} := T_1 \cdot r_{\text{intersect}} \frac{\gamma^{-1}}{\gamma}$$

 $T_2$  intersect = 600

$$T_{4\_intersect} := T_3 \cdot \left(\frac{1}{r\_intersect}\right)^{\frac{\gamma}{1}} \qquad T_{4\_intersect} = 600$$

at the r\_intersect the temperature out of the turbine matches the temperature out of the compressor, hence regeneration is infeasible

air-standard cycles ...

- 1. air as ideal gas is working fluid throughout cycle -no inlet or exhaust process
- 2. combustion process replaced by heat transfer process
- 3. cycle is completed by heat transfer to surroundings
- 4. all processes internally reversible
- 5. usually constant specific heat (page 311)

▶ reset variables

### Intercooled Brayton cycle



### example plot of intercooled Brayton cycle

parameters for plot. to retain states 2, 3 & 4 as previously defined two points 1a and 1b are inserted rather than renumbering. for intercooling,  $T_1 \Rightarrow T_{1a} \Rightarrow T_{1b} \Rightarrow T_2$ 

these are our assumptions for this analysis

$P_1 = P_{1a} = P_{1b} = P_2$			
s <sub>1</sub> => s <sub>1a</sub> => s <sub>1b</sub> =>s <sub>2</sub>			
starting conditions	$p_{1\_plot} := 1$	$T_{1_plot} := 25 + 273.15$	$s_{1_plot} := 1$
after first stage compression	$p_{1a\_plot} := \sqrt{10}$		
intercooler final temperature	$T_{1b\_plot} := T_{1\_plot}$		
after second stage compression	$p_{2\_plot} := 10$		
max temperature after heat addition	$T_{3_plot} := 1000 + 27$	3.15	

calculations



### p-v Brayton cycle (rev.) 1 stg interclg





pressure ratio (overall)

▶ reset variables

0 4

2

3

pressure ratio

4

5

#### Intercooled Regenerative Brayton cycle

T3 = low temperature from first intercooler, T4 second compressor. additional stages replicated at T3 and T4 which = T1 and T2 respectively. T5 is turbine inlet



maximum

observe ..  $T_3 := T_1$ 

 $pr := 1.01 .. 5.01 \eta = 1$ 

and ...initial stage of q<sub>L</sub> is ...

start with 1+ as

mathematically

 $T_2 - T_1$ 

 $\chi := 1.667$  for these calculations

$$\eta_{\text{th}_{ic}} = 1 + \frac{Q_L}{Q_H}$$

taking advantage of constant cpo

intercooled only from above

 $\eta_{\text{th}_ic} = 1 - \frac{T_6 - T_1 + N \cdot (T_2 - T_1)}{T_5 - T_2}$ 

so thermal efficiency becomes

power:= 
$$\frac{\gamma - 1}{\gamma}$$
 N:= 2  
T<sub>2</sub>(pr, N) := r<sub>c</sub>(pr, N)<sup>power</sup>·T<sub>1</sub>

$$\begin{split} \eta_{th\_ic\_reg} &= 1 - \frac{T_2 - T_1 + N \cdot (T_2 - T_1)}{T_5 - T_6} = 1 - \frac{(N+1) \cdot (T_2 - T_1)}{T_5 - T_6} \\ T_6(pr) &\coloneqq T_5 \cdot \left(\frac{1}{pr}\right)^{power} \qquad r_a(pr, N) \coloneqq pr^{\frac{1}{N+1}} \\ \eta_{th\_ic\_reg}(pr, N) &\coloneqq 1 - \frac{(N+1) \cdot (T_2(pr, \ ) - T_1)}{T_5 - T_6(pr)} \end{split}$$

 $T_1 := 300$   $T_5 := 1200$ 

for all intercooled stages

 $Q_H = (T_5 - T_6)$ 

assume ...  $T_4 := T_2$ 



as ...

with

regeneration

regeration was derived above leaving T1/T3 now renumbered to T1/T5 explicit. so variable T1/T5 inserted in arguments

11/14/2005

### intercooling, reheating and regenerative



### example plot of intercooled Brayton cycle with reheat (and regeneration)

parameters for plot. to retain states 2, 3 & 4 as previously defined two points 1a and 1b are inserted rather than renumbering. for intercooling,  $T_1 \Rightarrow T_{1a} \Rightarrow T_{1b} \Rightarrow T_2$ 

 $\begin{array}{l} p_1 => p_{1a} => p_{1b} => p_2 \\ s_1 => s_{1a} => s_{1b} => s_2 \\ \text{for reheat return to } T_{3;} \quad T_3 => T_{3a} => T_{3b} => T_4 \\ p_3 => p_{3a} => p_{3b} => p_4 \\ s_3 => s_{3a} => s_{3b} => s_4 \end{array}$ 

starting conditions  $p_{1 \text{ plot}} \coloneqq 1$   $T_{1 \text{ plot}} \coloneqq 25 + 273.15$  $s_1$  plot := 1  $p_{1a \text{ plot}} := \sqrt{10}$ after first stage compression intercooler final temperature  $T_{1b \text{ plot}} := T_{1 \text{ plot}}$ after second stage compression  $p_{2 \text{ plot}} := 10$ max temperature after heat addition  $T_{3 \text{ plot}} := 1000 + 273.15$  $p_{3a \text{ plot}} := \sqrt{10}$ after first turbine expansion max temperature after reheat addition  $T_{3b plot} := 1000 + 273.15$ -calculations







figure later χ:= 1.667  $\frac{Q_L}{Q_H}$ for these calculations  $\eta_{\text{th}_ic_reh_reg} = 1 +$ T<sub>1</sub> := 300 maximum  $T_5 := 1200$ for ease of calculations assume ...  $T_4 := T_2$ number of reheat and as ...

taking advantage of constant cpo

observe ..  $T_3 \coloneqq T_1$ for all intercooled stages

T5 inlet to turbine, stages of turbine are at T5 - T6 for all, intercooling are the same so pressure ratios are identical

and upper and lower temperature for reheat are at T5 and T6

$$\eta_{\text{th}_ic\_reh\_reg} = 1 - \frac{(N+1) \cdot (T_2 - T_1)}{(N+1) \cdot (T_5 - T_6)}$$
   
N:= 2

$$\underset{\gamma}{\text{power}} \coloneqq \frac{\gamma - 1}{\gamma} \qquad \qquad \underset{\gamma}{\text{r}_{c}(\text{pr}, \text{N})} \coloneqq \text{pr}^{\frac{1}{N+1}} \qquad \qquad \underset{\gamma}{\text{T}_{2}(\text{pr}, \text{N})} \coloneqq \text{r}_{c}(\text{pr}, \text{N}) \stackrel{\text{power}}{\coloneqq} \text{T}_{1} \qquad \qquad \underset{\gamma}{\text{T}_{6}(\text{pr}, \text{N})} \coloneqq \text{T}_{5} \cdot \left(\frac{1}{\text{r}_{c}(\text{pr}, \text{N})}\right)^{\text{power}}$$

$$\eta_{\text{th\_ic\_reh\_reg}}(\text{pr}, \text{N}) \coloneqq 1 - \frac{(\text{N}+1) \cdot (\text{T}_2(\text{pr}, \text{N}) - \text{T}_1)}{(\text{N}+1) \cdot (\text{T}_5 - \text{T}_6(\text{pr}, \text{N}))}$$



## example plot of multiple intercooled Brayton cycle with multiple reheat (and regeneration

parameters for plot. to retain states 2, 3 & 4 as previously defined two points 1a and 1b are inserted rather than renumbering. for intercooling,  $T_1 \Rightarrow T_{1a} \Rightarrow T_{1b} \Rightarrow T_2$ 

 $p_1 \Rightarrow p_{1a} \Rightarrow p_{1b} \Rightarrow p_2$  $s_1 => s_{1a} => s_{1b} => s_2$ for reheat return to  $T_{3:}$   $T_3 \Rightarrow T_{3a} \Rightarrow T_{3b} \Rightarrow T_4$  $p_3 \Rightarrow p_{3a} \Rightarrow p_{3b} \Rightarrow p_4$  $s_3 => s_{3a} => s_{3b} => s_4$  $p_{1_plot} := 1$   $T_{1_plot} := 25 + 273.15$  $s_1$  plot := 1 starting conditions pressure ratio pr plot := 20n comp := 4number of compression stages ... intercooler final temperature T<sub>1 plot</sub> max temperature after heat addition  $T_{3 \text{ plot}} := 1000 + 273.15$ number of expansion stages ... n exp := 4max temperature after reheat addition T<sub>3 plot</sub>

calculations



### p-v Brayton cycle (rev.) interclg & rht

as number of reheat and intercooled stages increases, ideal efficiency should approach Carnot

$$\eta_{\text{th}\_carnot} \coloneqq 1 - \frac{T_1}{T_5}$$
  $N \coloneqq 1 ... 20$   $pr \coloneqq 5$ 

this calculation fixes pressure ratio overall = 5 and looks at variation with number of stages of intercooling and reheat (same)

